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A Techno-Economic Evaluation of Post-Combustion Carbon Capture Using Renewable Ammonia

PROBLEM

Post-combustion carbon capture (PCC) using conventional amine-based solvents like MEA involves high regeneration energy, solvent degradation, and environmental concerns. Aqueous ammonia offers a low-cost, renewable alternative, however, its implementation faces technical challenges such as ammonia slip and solid precipitation (ammonium bicarbonate), which can lead to equipment blockages and increased operational complexity.



GENERAL OBJECTIVE

To evaluate the technical and economic performance of aqueous ammonia-based PCC systems with different process configurations: Base case, Rich Solvent Flashing (RSF), Lean Vapor Compression (LVC), and a novel Crystallizer-based (CRY) setup treating flue gas from a gas-fired power plant.

PROPOSAL

The study employed Aspen Plus® simulations for modeling four PCC configurations as shown in Figures 1 to 4: a base case, RSF, LVC, and CRY. Each setup treated 350 t/h of flue gas using a 5 wt% aqueous NH₃ solution. Process parameters such as CO₂ capture rate, ammonium bicarbonate formation, reboiler duty, regeneration energy, and economic costs (CAPEX/OPEX) were analyzed. The CRY configuration also evaluated the production of AmBic as a valuable by-product.

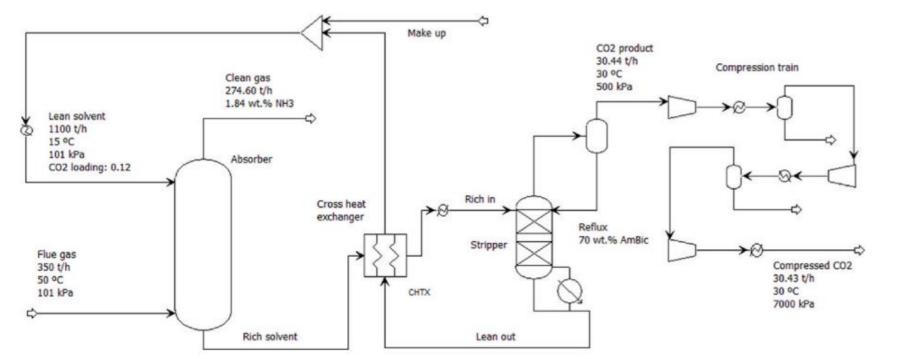
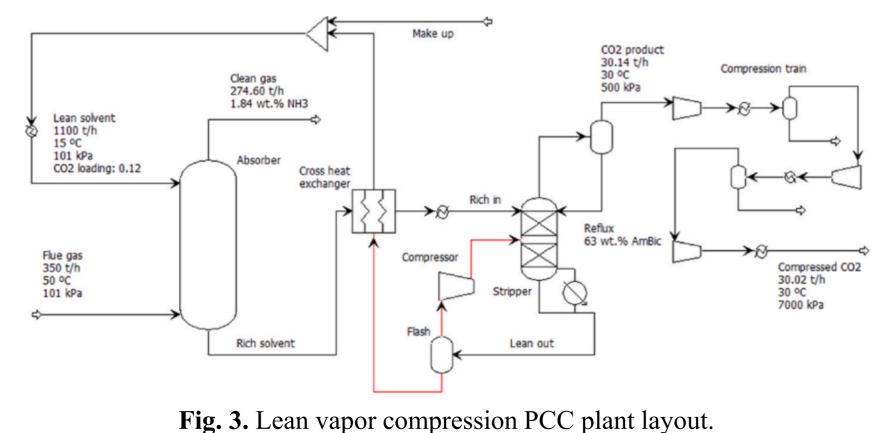


Fig. 1. Base case PCC plant layout.



29.04 t/h Compression train 274.60 t/h 1.84 wt.% NH3 1100 t/h CO2 loading: 0.12 Compressed CO2 350 t/h 27.61 t/h Lean out Fig. 2. Rich solvent flashing PCC plant layout. CO2 product 20.50 t/h 30 ℃ 500 kPa Compression train Clean gas 274.60 t/h 1.84 wt. % NH3 Lean solvent 1100 t/h Absorber Cross heat

Lean solvent

1100 t/h
1.84 wt. % NH3

Fiber

Rich solvent

Rich solvent

Fig. 4. CRY PCC plant layout.

RESULTS

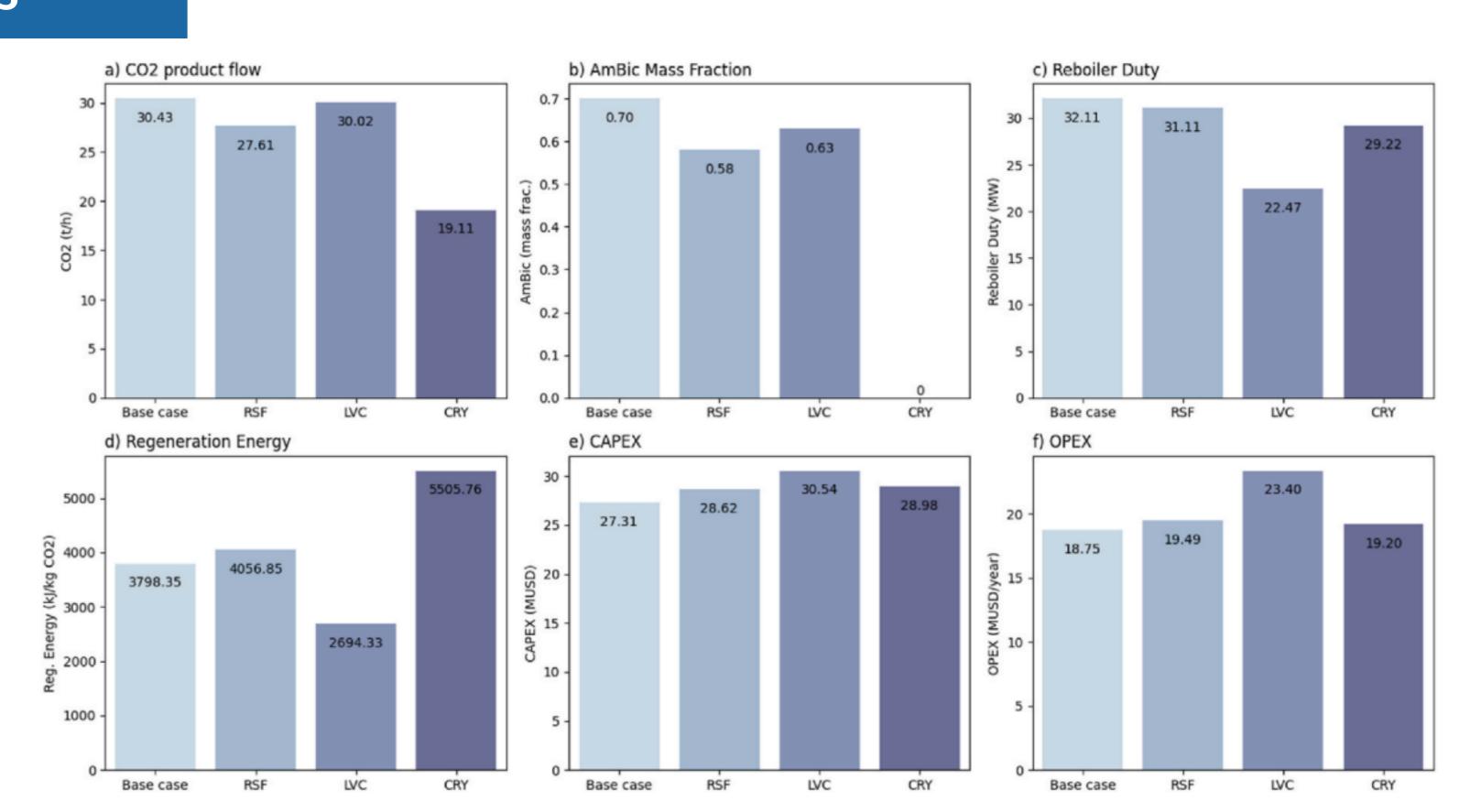


Fig. 5. Bar charts for the different key performance indicator. (5a-CO2 flow rate comparison, 5b-AmBic mass fraction comparison, 5c-Reboiler duty comparison, 5dRegeneration energy comparison, 5e-CAPEX comparison, and 5f-OPEX comparison).

CONCLUSIONS

- RSF offered modest improvement in AmBic reduction (−17.37%) and a slight decrease in reboiler duty (−3.10%), but also led to reduced CO₂ product flow while increasing CAPEX and OPEX
- LVC achieved significant energy savings, with a 30% reduction in reboiler duty and 29% lower regeneration energy. However, these gains came with the highest OPEX due to the additional compressor.
- CRY showed the lowest AmBic content (0%), eliminating precipitation risks in the reflux section. It reduced reboiler duty by 9%, though this was offset by a 37% drop in CO₂ flow and a 45% rise in regeneration energy due to CO₂ redirection for AmBic formation. However, AmBic recovery adds economic value, positioning CRY as a dual-benefit configuration.